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Behavior and Fate of Halloysite Nanotubes (HNTs) When Incinerating PA6/HNTs Nanocomposite

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ABSTRACT: Nanoclay-based nanocomposites have been widely studied and produced since the late 1990s, and frequently end up in waste disposal plants. This work investigates the behavior of PA6/HNTs nanocomposites (nylon-6 incorporating halloysite nanotubes) during incineration. Incineration tests were performed at lab-scale using a specific tubular furnace modified in order to control the key incineration parameters within both the combustion and postcombustion zones. The combustion residues and combustion aerosol (particulate matter and gas phase) collected downstream of the incinerator furnace were characterized using various aerosol analysis techniques. Time tracking of the gas and particle-number concentrations revealed two-step char formation during combustion. HNTs transformed into other mineral structures which were found in both the aerosol and the residues. During combustion of the polymer, it appears that



HNTs contribute to the formation of a cohesive char layer that protects the residual material.

2. INTRODUCTION

25 In recent decades, polymer nanocomposites have drawn much 26 attention due to their enhanced performance.¹⁻⁴ The physico-27 chemical properties of polymer matrices (tensile strength, 28 stiffness, heat resistance, barrier properties, etc.) are enhanced 29 by adding small amounts of nano-objects. This is the case with 30 polyamide 6 (PA6) incorporating silicate nanoclays. These 31 nanocomposites have been extensively studied and developed by 32 both universities and industry for many applications in various 33 industrial areas such as transportation, electronic and electrical 34 equipment, and packaging. Nevertheless, many of these state-of-35 the-art materials are expected to end up in waste treatment 36 facilities such as incineration plants due to the lack of specific 37 recovery procedures.⁵ Hence, the potential environmental risk 38 arising from the incineration of waste containing nanomaterials 39 is a new field which deserves further attention. Some recent 40 studies have begun to focus on this topic, but the data are $_{41}$ incomplete.⁵⁻¹² The present study therefore gives some insight 42 into the fate and behavior of nano-objects (incorporated in a 43 polymer matrix) during the incineration of nanocomposites. The 44 work focuses on PA6/HNTs nanocomposites (nylon-6 incor-45 porating halloysite nanotubes).

46 Polyamide 6 (also called Nylon-6) is a semicrystalline 47 polyamide thermoplastic used in a wide range of fiber, film and 48 engineering applications. It has been shown that a small amount (1–10 wt %) of silicate nanofiller can remarkably enhance the 49 properties of the material.^{2,13} Nanofillers based on montmor-50 illonite layered silicates have been the subject of many studies. 51 More recently, halloysite nanotubes (HNTs) have also been 52 studied, and have been reported to improve many properties, 53 especially thermal properties, when incorporated in a PA6 54 polymer matrix.^{14–17} HNTs are alumino-silicates. Their 55 chemical composition is $Al_2Si_2O_5(OH)_{4,2}H_2O$. They are 56 extracted from natural deposits and are chemically similar to 57 kaolinite. Their nanotubular structure gives them very interesting 58 properties that attract the attention of researchers for many 59 applications.^{17–19}

Many articles and book chapters have been published about 61 the thermal degradation of nanocomposites, ^{13,16,20–25} but none 62 of them relate to tests involving the combustion parameters of 63 incineration (temperature around 850 °C, highly ventilated 64 combustion, at least 2 s residence time for the combustion gas in 65 a postcombustion chamber at 850 °C, and high oxygen/fuel 66 contact) or time tracking of the gas and particle concentrations 67 in the combustion aerosol. In the present work, we used a 68 69 laboratory scale furnace modified to control the key incineration 70 parameters. The combustion aerosol was sampled downstream 71 of the postcombustion chamber (i.e., analogous to upstream of 72 filtration in a real-scale incineration plant), and was characterized 73 using various aerosol analysis techniques. This was a first step in 74 the evaluation of the efficiency of flue-gas cleaning systems. After 75 that, the combustion residues were analyzed. The aim of this 76 work is to study the behavior and the fate of HNTs during 77 incineration of PA6/HNTs nanocomposites while investigating 78 the influence of HNTs on combustion mechanisms (aerosol 79 release and decomposition) and the release of nano-objects 80 during incineration. It is relevant to ask whether the nano-objects 81 initially incorporated in the polymer are destroyed or undergo 82 changes during their stay in the incinerator and their fate 83 thereafter.

3. MATERIALS AND METHODS

3.1. Sample Preparation and Characterization. PA6/ 85 HNTs nanocomposites (see Supporting Information (SI), 86 Table S1) were prepared by melt extrusion and injection 87 molding. The halloysite (shown in Figure 1) was provided by



Figure 1. Pristine HNTs dispersed in PA6/HNTs nanocomposite.

88 Imerys Ceramics from New Zealand. PA6 (polyamide 6) 89 Technyl C206 was supplied by Rhodia Plastics Engineering 90 SA. Neat matrix and two nanocomposites at two loadings (1 and 91 5%wt) of HNTs were prepared using the same extrusion and 92 injection process to ensure the same thermo-chemical history for all samples. A twin-screw extruder (Clextral BC21, 1200 mm 93 length) was used (rotational speed of 250 rpm, and processing 94 temperature of 260 °C). The pelletized extruded material 95 obtained was finally injection molded (Krauss Maffei KM50/ 96 180CX) into standard specimens ($100 \times 100 \times 4 \text{ mm}^3$). 250 mg 97 samples from these specimens were cut and then tested in the 98 incinerator furnace.

The pristine HNTs and the prepared nanocomposite samples 100 were characterized prior to the incineration tests. Imagery on 101 pristine HNTs and on the dispersion of HNTs in the nano- 102 composite (Figure 1) was carried out using transmission elec- 103 tronic microscope (Philips CM12 TEM 200 kV). In addition, 104 elemental analysis of the polymer material, laser diffraction and 105 X-ray fluorescence analysis of pristine Halloysite were performed 106 (see SI, Tables S2 and S3 and Figure S2). TEM micrographs 107 show the nanotubular structure of the pristine halloysite (Figure 1). 108 In agreement with literature, ^{14–18} the observed halloysite tubes 109 are nanosized with a thickness lower than 100 nm. 110

Thermogravimetric analysis (TGA) was performed using a 111 Pyris-1 Perkin–Elmer apparatus. Samples of 10 (\pm 2) mg were 112 heated under a nitrogen flow at a 10 °C/min heating rate from 113 ambient temperature to 850 °C. 114

PCFC (pyrolysis combustion flow calorimeter) tests were 115 carried out using a fire testing technology apparatus (FTT, 116 ASTM D7309). A sample of 2 (\pm 1) mg was heated under 117 nitrogen flow to 750 °C at a heating rate equal to 1 K/s. Gases 118 were extracted and sent to a combustion chamber in the presence 119 of a N₂/O₂ flow (80/20). The combustor ensured complete oxida-120 tion of pyrolysis products at a combustion temperature fixed at 121 900 °C.²⁶ 122

3.2. Lab-Scale Incinerator and Analysis. Laboratory scale 123 incineration tests were performed using a specific tubular 124 furnace. The combustion conditions implemented in the lab-125 scale incinerator furnace (within both the combustion and 126 postcombustion zones) were controlled to satisfy the key 127 operational parameters that govern an incineration process, 128 that is, chiefly temperature (850 °C in the combustion and 129 postcombustion-zone), residence time (at least two seconds in 130 the postcombustion zone at 850 °C), air-excess (never below 131 11% of oxygen) and turbulence (a good mix between 132 combustible and oxygen). A tubular horizontal furnace 133 (Carbolite STF 15/610 Horizontal Tube Furnace) was modified 134 to obtain as close as possible to the combustion conditions 135 implemented in an industrial grate incinerator. As illustrated in 136



Figure 2. Basic diagram of the modified tubular furnace—Lab-scale incinerator and the measurement lines.

¹³⁷ Figure 2 the "combustion chamber" is maintained at 850 $^{\circ}$ C ¹³⁸ (at least) and where air cross flows penetrate and mix with the ¹³⁹ combustibles. Then, the "post-combustion chamber" is the ¹⁴⁰ furnace zone where the combustion aerosol stays 2 s at 850 $^{\circ}$ C ¹⁴¹ (at least).

Finally the combustion released gases and the aerosol particles relation to the measurement line as described in the relation of the second paragraph.

In order to superimpose the curves of time tracking, it is in the important to know the response time of each measurement into synchronize all events detected. The reaction time of each unit of the measurement line is determined by stopwatch. An ucertainty of two seconds is taken into account.

The combustion aerosol was sampled appropriately as 151 explained below and analyzed in three different ways: time 152 tracking for the gas and particles from the aerosol and two off-line 153 analyses for the particulate matter. Further analyses were 154 conducted on the combustion residues.

3.2.1. *Time Tracking for the Gas Phase.* The sampling of the sampling direct emissions from stationary combustion used for sampling direct emissions from stationary combustion sources. The flue gas leaving the furnace was dried and filtered using a line with a hot filter and a condenser. A multigas analyzer (portable gas analyzer PG-250 Horiba) was used. It indicates the evolution of the combustion gases concentrations: the consumption of O₂ ($%_{vol}$.) and the production of NOx (ppm_{vol}.), GO₂ ($%_{vol}$.) and CO (ppm_{vol}.). They are respectively detected by paramagnetism, chemiluminescence and an infrared technique swith 1 s time resolution.

166 3.2.2. Time Tracking and off-Line Analysis for Particulate 167 Matter. The combustion aerosol sampled downstream of the 168 postcombustion chamber has to be representative of the aerosol 169 sampled upstream of the flue-gas cleaning systems. The target 170 temperature is 170 (\pm 10) °C. In fact, under industrial conditions, 171 the aerosol leaves the postcombustion chamber and goes 172 through an upstream filtration processes at a temperature 173 around 150 °C in accordance with BREF Waste Incineration 174 (2006).²⁷ Different samplers and impactors were used to 175 conduct the analyses with respect to the temperature constraint 176 mentioned above.

Regarding the time tracking of the particles from the 177 178 combustion aerosol, an electrical low pressure impactor, Dekati 179 (ELPI) was used downstream of a fine particle sampler dilutor 180 (FPS, Dekati). The objective of the sampling was to avoid cold 181 spots below 170 °C before and during the first dilution. FPS 182 dilutor is well adapted to measurements related to combustion 183 research. This system allows sampling from hot flue gas and 184 provides controlled temperature decrease with minimal 185 losses.^{28–30} The FPS dilutor performs two successive dilutions: 186 the first heated dilution at 170 °C and the second at room tem-187 perature. The primary dilution air was heated to 170 (± 10) °C. 188 Thus, the sampled combustion aerosol underwent two dilutions 189 with a total factor of 1:30. The dilution ratio was given in real 190 time by the FPS software. However, in order to check the 191 displayed FPS value, the dilution ratio was recalculated 192 continuously during the test using a gas analyzer connected to 193 the output the FPS which indicates the concentration of CO and 194 CO₂ after the dilution.³¹

The ELPI provided a real-time measurement of particle num-196 ber concentration through 12 channels from 17 nm to 5 μ m.³² 197 The PN_{x-y} are defined as the number concentration of particles 198 counted by the ELPI with mean geometric diameter (Di) 199 between x and y μ m. Regarding off-line analyses, there were two types of sampling: 200 in the first type, combustion aerosol particles were collected 201 throughout the test; in the second type, combustion aerosol 202 particles were collected over a targeted time range. 203

In the first case, the aerosol combustion underwent just one 204 hot dilution at 170 °C with a porous tube dilutor from VTT 205 laboratory (Valtion Teknillinen Tutkimuskeskus Technical 206 research center of Finland).³³ This diluted hot sample was 207 routed to a gravimetric impactor (DGI, Dekati Gravimetric 208 Impactor) which was heated to the same temperature (170 $^{\circ}C \pm 209$ 10 °C). This PM_{2.5} four-stage impactor resolves particles into 210 four size fractions with 50% collection efficiency for aerodynamic 211 (dp50) cut-points of 2.5, 1.0, 0.5, 0.2 μ m plus a back-up filter 212 (after the impaction stages) which collects all particles typically 213 smaller than 0.2 μ m.³⁴ In this way, the particulate matter of 214 the combustion aerosol was collected on PTFE impaction 215 substrates with controlled temperature during sampling. Then, 216 these particles were analyzed by a scanning electronic micro- 217 scope (JEOL 7600F High Resolution Analytical SEM energy 218 dispersive spectrometer SDD BRUKER (EDS) X-ray detector). 219 This gravimetric impactor provided a qualitative analysis 220 (imagery and chemistry) of particles collected during the 221 whole combustion test. 222

In the second case, particles from the combustion aerosol were 223 collected on a TEM grid for above 10 s downstream of the tubular 224 furnace with a MPS (Mini-Particle-Sampler, Ecomesure³⁵). A 225 Philips CM12 TEM 200 kV was used for the imagery. 226

3.2.3. Analysis of the Combustion Residues. The combus- 227 tion residues in the sample holder of the lab-scale incinerator 228 were collected after each test. They were analyzed by TEM 229 (Philips CM12 TEM 200 kV), and SEM. X-ray diffraction 230 (XRD) with a Bruker AXS D8 Advance diffractometer using Cu 231 K α radiation. 232

4. RESULTS

4.1. Time Tracking of Gas Concentration and Particle 233 Number Concentration. The graphs showing the evolution of 234 concentrations during the incineration of the nanocomposite 235 PA6/5HNTs are given in Figure 3a. The two verticals delimit 236 the time range with more than 5% O_2 consumption from the 237 baseline. This area of interest is denoted "AOI". The averages of 238 three runs are presented with the associated standard deviation. 239 When the neat matrix is compared to the nanocomposite, weight 240 standardization was performed in order to compare the same 241 mass of polymer. 242

Before the AOI, from 0 to 48 s, O_2 consumption is low, little 243 gases are produced, but particles are strongly emitted with a 244 domination of PN_{0.1}. Ignition is observed during this period. 245 During the AOI, which extends over a period from 48 to 100 s, 246 oxygen consumption is maximal. From 48 to 80 s, peaks of CO₂, 247 CO and NOx are noticed while PN_{x-y} decreases. From 80 to 248 100 s, a second peak of CO begins along with an increase in 249 PN_{0.1}. After the AOI, from 100 s to the end (250 s) a shoulder in 250 NOx concentration appears with a second peak of CO, particles 251 are less and less emitted, and O₂ reaches its baseline.

High concentration levels are noticed here. Then, considering 253 such high concentrations, coagulation/agglomeration phenom- 254 ena must occur in the furnace. Even if the pilot does respect a 255 residence time of two seconds, it would be difficult to say if these 256 phenomena occur in a real scale industrial furnace. This is rightly 257 a limit of an incinerator lab-scale pilot. 258

Figure 3b-d show the comparisons between neat PA6 and 259 PA6/SHNTs nanocomposite. A second phase of particle 260



Figure 3. (a) Time tracking for PA6/SHNTs incineration: particle number concentration and gas concentration, (b) Comparison between PA6 and PA6/SHNTs for PN_{0.1} concentration, (c) Comparison between PA6, PA6/SHNTs and PA6/1HNTs for CO concentration, (d) Comparison between PA6 and PA6/SHNTs for NOx concentration (log scale).

 261 emission is clearly observed, as well as a shoulder in NO_x 262 concentration and a second peak of CO but only for 263 nanocomposite. This tendency is the same for PA6/1HNTs

(Figure 3c) with its CO curve just inserted between the two other 264 CO curves. Other time tracking comparisons show no significant 265 differences (see SI, Figures S3 and S4). 266



Figure 4. (a) Combustion aerosol particles collected on PTFE impaction substrate: soot and HNTs*, (b) Combustion aerosol particles collected on TEM grid: soot and HNTs* aggregates, (c) Combustion residues: HNTs* aggregates and individual HNTs*.

4.2. Imagery. The results from imagery provide only qualitative considerations.

²⁶⁹ HNTs* are defined as pseudo-HNTs with transformed ²⁷⁰ mineral structures from HNTs.

4.2.1. Combustion Aerosol Particles. Imagery on particles 271 collected on PTFE impaction substrates reveals the presence of 272 HNTs* among the soot particles as shown in Figure 4a. These 273 particles are from the fourth stage with dp50 = 1 μ m. Submicron 274

275 HNTs* aggregates represent a minor fraction. Figure 4b shows 276 the particles collected on a TEM grid during ten seconds 277 preceding AOI. Submicron HNTs* aggregates are also minor 278 components among the soot particles.

4.2.2. Combustion Residues. TEM and SEM (coupled with X-ray microanalysis) performed on combustion residues reveal that the residues are entirely inorganic and seem to consist of mineral aggregates and individual mineral particles (Figure 4c). No residues remain for the neat matrix case since neat PA6 decomposes completely.

4.2.3. TGA and PCFC on Nanocomposite. Figure 5 presents TGA curves of neat matrix, pristine HNTs and PA6/5HNTs.



Figure 5. TGA under N₂.

²⁸⁷ The mass loss of HNTs (14%wt) corresponds to water release ²⁸⁸ and occurs mainly in the 350–600 $^{\circ}$ C range. The mass loss range ²⁸⁹ of PA6 occurs between 350 and 500 $^{\circ}$ C. It can be noticed that the ²⁹⁰ presence of HNTs reduces the degradation onset temperature ²⁹¹ and the thermal stability up to 450 $^{\circ}$ C.

The incorporation of HNTs in PA6 reduces the PCFC peak (463 W/g for the pristine PA6 and 459 W/g for the composite). Besides, the shift toward high temperatures is almost unnoticeable because it is correlated with a mixing law (Figure 5). Nevertheless, PCFC peaks coincide roughly with the derivates of TGA curves (Figure 5, Figure 6). For both techniques, the thermal degradation of PA6 occurs at lower temperatures in the presence of HNTs.

4.2.4. XRD on Pristine HNTs and Residues. For pristine HNTs, X-ray fluorescence analysis (SI Table S3) and X-ray diffraction pattern (Figure 7) highlight that quartz (cristobalite) so is present (nodular shape) as impurity of halloysite. The presence



Figure 6. Heat Rate Release at PCFC of neat matrix and PA6/5HNTs nanocomposite.



Figure 7. XRD of pristine HNTs and residues of nanocomposites.

of quartz leads to an excess of silicon over aluminum, since in 304 pure halloysite, their ratio is 1:1. 305

XRD spectra performed on residues show that they essentially 306 contain cristobalite and quartz. A bump can be noticed for the 307 residue from PA6/5HNTs (between $2\theta = 20$ to 30°) which can 308 be ascribed to an amorphous alumino-silicate structure. Only a 309 peak at 44° was not identified. A temperature of at least 850 °C 310 is attained in the furnace. Consequently, no halloysite remains 311 in the residue even if SEM micrographs show pseudotubular 312 structures, also for individual particles. 313

5. DISCUSSION

Considering the results about time tracking and imagery, 314 interpretations can be proposed concerning the behavior and 315 fate of HNTs during the incineration of PA6/HNTs nano- 316 composites. 317

5.1. HNTs Behavior: A Two Step Mechanism. First of all, 318 a clear difference exists between the neat matrix and the 319 nanocomposite. A two-step mechanism can be considered for 320 PA6/HNTs nanocomposite. The evidence for this is the second 321 CO peak, the NO_x shoulder, and the second phase in the 322 emission of particles. Thus, the presence of HNTs is clearly 323 responsible for this two step mechanism. 324

It takes around 15 s to introduce the sample in the furnace. 325 326 This step involves particle emissions due to aerodynamic 327 disturbance from the set up and due to the first thermal effects 328 on the sample. Then, from 15 to 50 s, the thermal decomposition 329 of the sample is indicated by the release of gases and particles, and 330 by the presence of a flame for a few seconds. Effectively, as shown 331 by TGA (Figure 5), HNTs lose water, so a hydrolysis of PA6 332 occurs and there is an increase in the release of volatile 333 combustibles.³⁶ Furthermore, during this step, according to the 334 literature, it is assumed that due to the thermal ablation of the 335 polymer and the dehydration of HNTs, decohesion occurs ³³⁶ between the PA6 and the HNTs.^{25,37} Through these processes, 337 the HNTs concentration at the surface of the sample increases 338 and a protective layer gradually forms. TEM observation of 339 particles collected during this phase reveals the presence of 340 HNTs (in small quantities). The high concentration at the 341 surface would promote the release of HNTs and make them free 342 from the matrix and able to be carried away by the aerosol flow. As reported in the literature, polyamide 6 could be considered 344 as a charring polymer and the nanoclays as char promoters.^{24,38} 345 In fact, during a thermal decomposition, some materials can 346 develop on their surface a protective layer which limits mass 347 transfer (volatile combustible and oxygen transfer) as well as 348 thermal transfer. Actually, CO time tracking with a double peak is 349 a good indicator of the protective layer evolution. It was 350 established that the decomposition of charring polymer involve 351 two phases of gas release: the first one is associated with the 352 primary char formation and the second one with the 353 decomposition of the nonstable primary char.^{39,40} Hence in 354 the present case, the protective layer can be made of a 355 carbonaceous char reinforced by HNTs. This char/HNTs layer 356 forms progressively, since under-ventilated combustion occurs 357 with a significant increase in CO emissions (Figure 3c). 358 Simultaneously, the particle emission decreases from 45 s up to 359 70 s (Figure 3a) which is in agreement with the formation of a 360 cohesive char layer. After 65s which corresponds to a CO peak, 361 CO emission decreases and reaches a local minimum while 362 oxygen consumption rises dramatically. This corresponds to the 363 oxidation of the primary char.^{39,40} Moreover, this oxidation is 364 accompanied by an increase in particle emissions, which is 365 irregular and suggests a partial cracking of the protective layer. So 366 the second peak of PN_{0.1} reflects the presence of a second 367 combustion event. Furthermore, the NO_x shoulder from 100 s 368 reflects the oxidation of the residual material which is no longer 369 protected by the cracked char/HNTs layer (Figure 3d).

At the end of the combustion test, the residues from PA6/ 371 SHNTs incineration consist only of mineral compounds derived 372 from the initial HNTs objects. However, some studies report 373 carbon/clay residues after pyrolysis tests on polymer/clay 374 nanocomposites³⁷ and especially for PA6/HNTs nanocompo-375 sites.¹⁶ This difference should come from the combustion 376 conditions implemented in the furnace. In fact, in our case the 377 sample is well oxygenated at high temperature (850 °C or more) 378 and for a high rate of increase in temperature (from 25 to 850 °C 379 in 10 s). Therefore, under our incineration conditions, combus-380 tion is complete and no organic residues remain in the sample 381 holder.

As with other nanoclays (montmorillonite for example), HNTs are known to have fire-retardant properties when inter a polymer matrix.^{16,17} During exposure to a heat source, these refractory materials can protect the matrix in which they are incorporated through the formation of a protective clay barrier which acts as a screen toward mass and heat transfers. The fire retardancy conferred by HNTs is confirmed by both the 388 reduction in the peak heat release rate (pHRR) observed with the 389 PCFC and the two-step mechanism discussed above. But this 390 retardant character is not effective enough since it has been 391 established that more than 15%wt is necessary to meet fire 392 retardancy standards for industrial applications.¹⁶ 393

The comparison between neat PA6 matrix and PA6/SHNTs 394 nanocomposite shows that CO emission is stronger for the 395 nanocomposite with a first peak at lower time. Besides, this 396 tendency is confirmed for PA6/1HNTs (Figure 3c) with its CO 397 curve just inserted between the two other CO curves. This 398 suggests better char formation in the presence of HNTs. This 399 easier char formation could be related to the lower thermal 400 stability for the composite shown by TGA and PCFC, which 401 indicate that the release of water from the clays leads to 402 hydrolysis of PA6 polymer chains. Since the emission of particles 403 is significantly lower for neat PA6, it shows that the char is more 404 unstable with the unfilled polymer, and burns more easily.

We can thus surmise that the HNTs modify the thermal 406 behavior of the PA6/HNTs nanocomposite during its 407 incineration and that the more HNTs incorporated in PA6, the 408 more the phenomenon is accentuated. In fact, these nanoclays 409 enhance PA6's ability to form a protective char layer, and 410 reinforce it via a cohesive char/HNTs layer. To sum up, through 411 a two-step mechanism as suggested by analysis of the time 412 tracking, this char/HNTs layer gradually forms, acts as a barrier, 413 cracks, oxidizes and ends up entirely inorganic. 414

5.2. Fate of HNTs: Aggregates in Aerosol and Residues. 415 The imagery results reveal the presence of mineral nano-objects 416 in both the combustion aerosol and the combustion residues as 417 aggregates and as prismatic (pseudotubular) structures which 418 could result from partial distortion of the tubular structure. 419

Thus, HNTs are not destroyed during the incineration of 420 PA6/HNTs nanocomposites, but seem to be transformed into 421 other mineral structures (named HNTs*). Only qualitative 422 considerations can be discussed here. 423

At high temperatures (beyond 1000 °C), the tubular 424 morphology tends to distort and then halloysite transforms 425 into new crystalline or amorphous structures such as gamma- 426 alumina, cristobalite, and mullite.⁴¹⁻⁴³ Actually, it is established 427 that thermal decomposition of HNTs occurs in three steps: 428 dehydration (loss of H₂O from \sim 200 °C), dehydroxylation (loss 429 of OH from ~500 to 900 °C) and a mullite-like phase formation 430 (from 1200 to 1400 °C). The distortion of the tubular structure 431 begins from 1000 °C and fusion up to 1400 °C.⁴¹⁻⁴³ Considering 432 the high temperatures reached in the furnace (at least 850 °C and 433 more in the presence of a flame), the HNTs undergo the 434 aforementioned thermal transitions during the incineration of 435 PA6/HNTs. Thus, the presence of mineral aggregates identified 436 as pseudo-HNTs with transformed mineral structures (HNTs*) 437 could be explained by the thermal process occurred during the 438 HNTs' stay in the furnace, and the aggregated state could also be 439 explained by a sintering process occurring during the stay above 440 850 °C. Nevertheless, the temperature is not high enough to 441 ensure the crystallization of mullite. 442

Finally, regarding the behavior of multilayered silicates, it can 443 be suggested that for the incineration of other PA6/silicate 444 nanocomposites, mineral nano-objects could be found both in 445 the aerosol downstream of the postcombustion chamber and in 446 residues, but possibly transformed into other mineral structures, 447 taking into account the temperature of the incinerator and the 448 residence time. This should be confirmed by prospective 449 additional incineration tests on other nanocomposites. 450 **5.3. Concerns about Incineration of Waste Containing 5.2 Nanomaterials.** A nanomaterial can be defined as any **5.3 intentionally manufactured material, containing particles, in an 5.4 unbound state or as an aggregate or as an agglomerate and where, 5.5 for 50% or more of the particles in the number size distribution, 5.6 one or more external dimensions is in the size range 1–100 nm, 5.7 according to the European Commission article 18(5) of 5.8 Regulation 1169/2011. 5.4 Their potential releases in the 5.9 environment during their life cycle and their subsequent impacts 5.6 on health have been an increasing concern for many years.** Toxic **5.6 different types of nanomaterials have been studied and 5.6 demonstrated. 5.7 detailed studies are required.**

The aim of the present study was to provide an insight into hazards regarding the incineration of waste containing nanomaterials from nanocomposites. Therefore, lab-scale tests were performed to investigate the release of nano-objects downstream objects in slag residues. Nano-objects from nanocomposites were objects in slag residues. Nano-objects from nanocomposites were found in the combustion aerosol and in residues. This leads to after the conclusion that both flue gas and slag treatments would be after affected by concerns about nanomaterial incineration and the presence of the

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482 Notes

483 The authors declare no competing financial interest.

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